

**IN THE CLAIMS:**

1. (Amended) Method for manufacturing menthol by catalytic hydration of starting materials having the carbon network of menthane with at least one double bond and which are substituted in 3-position by oxygen and/or catalytic rearrangement of stereoisomers of the menthol in the presence of hydrogen, characterised in that the reaction is performed in the presence of a nickel catalyst doped with iron and/or chromium and at a temperature in the range 80-230°C and hydrogen pressures in the range 1-200 bar abs., whereby the doped nickel catalyst in the dry state has an iron content of 0.1-20% by weight, a chromium content of 0.1-20% by weight, a nickel content of 60-95% by weight and an aluminum content of 1-20% by weight.
2. (Amended) Method according to Claim 1, characterised in that the ~~iron or chromium doped nickel catalysts have~~ catalyst has an iron or chromium content of between 0.1 and 20% by weight in relation to the dry catalyst. content of 0.1-10% by weight, a chromium content of 0.1-10% by weight, a nickel content of 80-93% by weight and an aluminum content of 3-10% by weight.
3. (Amended) Method according to Claim 1 ~~or 2~~, characterised in that the ~~nickel catalyst in the dry state has an iron content of 0.1-20% by weight, a chromium content of 0.1-20% by weight, a nickel content of 60-95% by weight and an aluminium content of 1-20% by weight.~~ method is essentially performed without diluent.
4. (Amended) Method according to ~~at least one of Claims 1 to 3~~ Claim 1, characterised in that the nickel catalyst in the dry state has an iron content of 0.1-10% by weight, a chromium content of 0.1-10% by weight, a nickel content of 80-93% by weight and an aluminium content of 3-10% by weight.
5. (Amended) Method according to ~~at least one of Claims 1 to 4~~ Claim 1, characterised in that the ~~method is essentially performed without diluent.~~ reaction temperature is between 120 and 210°C.
6. (Amended) Method according to ~~at least one of Claims 1 to 5~~ Claim 1, characterised in that the ~~weight ratio between the dry nickel catalyst and the starting materials is in the range 0.001-0.1;~~ method is performed discontinuously.
7. (Cancelled)

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8. (Cancelled)
9. (Amended) Method according to Claim [[8]] 6, characterised in that the hydrogen pressure is between 3 and 50 bar abs.